AMENDMENTS TO THE SPECIFICATION:

Please replace the paragraph beginning at page 3, line 1 with the following amended paragraph:

In this regard, processes for producing iodo ~~aklynyl~~ alkynyl carbamates are ~~know~~ known. For example, U.S. Patent No. 5,693,849, issued on December 2, 1997 (the '849 patent), relates to a process for producing iodo alkynyl carbamates. The process is carried out in an aqueous environment which comprises an aqueous solution of a surfactant, which can be either an acidic organic phosphate partial ester or a sulfated fatty alcohol. These are ionic surfactants. A alkynyl carbamate is dispersed in the aqueous reaction medium and iodinated with iodine in the presence of sodium hypochlorite. Among other things, the process of the present invention is distinct from the process of the '849 patent in that, in the subject invention, the surfactant is preferably nonionic. Further, the surfactant used ~~is~~ in the '849 process are of two carefully defined classes of phosphated or sulfated compounds, and lastly the carbamate is iodinated with elemental iodine. Specific surfactants are stated to be required for the reaction of the carbamate with elemental iodine.

Please replace the paragraph beginning at page 7, line 1 with the following amended paragraph:

In the reaction, a suitable reactor is charged with an amount of the surfactant solution and the charge is cooled to a temperature of from about 0 to about 8°C or to a temperature of from about 0 to about 12°C; [[,]] a more preferred range for this temperature is from about 5 to about 12°C , with a most preferred range being from about 8 to about 10°C and a most preferred operating temperature being 9°C. If these temperature parameters are varied, the yield and quality of the IPBC formed may be adversely affected.

Please replace the paragraph beginning at page 7, line 14 with the following amended paragraph:

The reactor must have a molar ratio of alkali to match the molar concentrations of n-propynyl butylcarbamate which will be subsequently charged to the reactor mass. From about 0.8 to about 1.0 moles of alkali per mole of n-propynyl butylcarbamate should be provided.

Please replace the paragraph beginning at page 8, line 17 with the following amended paragraph:

With the addition of the oxidizing agent the reaction is essentially complete. ~~The~~ While agitating, the reaction mass is allowed to slightly increase in temperature, to allow for complete iodination of the propynyl butylcarbamate. At this stage of the reaction the temperature should not exceed 20°C. The temperature usually ranges from about 15 to about 20°C. If the temperature at this stage of the reaction exceeds 20°C the quality of the resulting IPBC is adversely affected.

Please replace the paragraph beginning at page 8, line 22 with the following amended paragraph:

While stirring, the reaction is allowed to proceed for a period of time of from about 30 to about 180 minutes; in an embodiment, the reaction proceeds for from about 60 to about 120 minutes. A most preferred reaction time is 90 minutes. Reaction times of longer than 180 minutes result in lower yield and quality of the resulting IPBC is adversely affected. If the reaction time is allowed to exceed 180 minutes, some of the iodine may be stripped off of already formed IPBC producing off colored and undesirable isomers.

Please replace the paragraph beginning at page 9, line 2 with the following amended paragraph:

At this point, the conversion of propynyl butylcarbamate to IPBC is essentially complete. The temperature of the reaction mass is then allowed to ramp up to a temperature of from about 35 to about 40°C at a rate of from about 0.25 to about 1.0 degrees per minute or a rate of from about 0.25 to about 0.75 degrees per minute.

Please replace the paragraph beginning at page 9, line 7 with the following amended paragraph:

The pH of the reaction mass is then adjusted with an organic acid such that the pH of the reaction mass is slightly acidic. In one embodiment, the reaction mass is adjusted to a pH of about 6.9 with an organic acid, preferably with acetic acid. The pH is then adjusted to about 6.6 using a mild acid buffer such as sodium bisulfite.

Please replace the paragraph beginning at page 9, line 10 with the following amended paragraph:

The temperature of the reaction mass is allowed to further ramp up to a temperature of from about 55 to about ~~58~~ 59°C, with a most preferred range being from about 55 to about 56°C. This temperature ramp up is effected at a rate of from about 0.25 to about 0.75 degrees per minute.

Please replace the paragraph beginning at page 9, line 14 with the following amended paragraph:

When this ramp up in temperature is effected to the desired range, the temperature of the reaction mass is immediately ramped downward to a range of between 20 and 30°C, or more preferably a range of between 25 and 30°C , with a most preferred temperature being 25°C. The ramping down of the temperature is effected at a rate of from about 0.25 to about 0.75°C per minute or from about 0.35 to about 0.75°C per minute. Agitation continues during this ramp down.

Please replace the paragraph beginning at page 12, line 17 with the following amended paragraph:

The reactor with strong agitation was slowly charged with 1780 pounds of a 13.6% solution ~~of sodium~~ of sodium hypochlorite while maintaining the reaction mass at a temperature of between 6 and 11°C.

Please replace the paragraph beginning at page 12, line 24 with the following amended paragraph:

With agitation the pH of the reaction mass was then adjusted to 6.9 with acetic acid. The pH reaction mass was then adjusted to 6.6 with sodium bisulfite. The temperature was then ~~tamped~~ ramped up to 55 to 59°C at a rate of 0.25 to 0.75°C per minute.